

Esterification of Glucose by Coconut Oil Fatty Acids Using Immobilized *Candida rugosa* Lipase E.C.3.1.1.3. in Ca-alginate Matrix

Sri Handayani, Syarifah Hasna, Siswati Setiasih, Sumi Hudiyo*
Departement of Chemistry, Faculty of Mathematics and Science, University of Indonesia
Kampus UI Depok 16424, Indonesia

Abstract: In this study, the synthesis of fatty acid – carbohydrate esters used glucose (G) and coconut oil fatty acid (FA). The esterification reaction was carried out enzymatically using *Candida rugosa* lipase in organic solvent (n-hexane). Lipase was immobilized on Ca-alginate gel beads with the optimum condition for immobilization was 1 % of Na-alginate, resulting 61.66% immobilization yield. The optimum conditions for esterification using immobilized lipase in Ca-alginate were at 35°C, the molar ratio 1:60 (G/FA), 16 hours incubation time and 0 g molecular sieve. Characterization of synthesized product with FT-IR showed that product exhibit the absorption of ester functional group at 1737 cm⁻¹, but with the greater OH group absorption peak at 3344.57 cm⁻¹ indicated that the degree of esterification was still low. The synthesized product was then examined by simple emulsion test and was proved to be an emulsifier. Based on the emulsion test, it was known that the products of the reaction were glucose esters that have properties amphiphilic as an emulsifier system of oil-in-water emulsion (o/w).

Keywords: glucose ester, *Candida rugosa* lipase, lipase immobilization, Ca-alginate, coconut oil fatty acid

I. Introduction

Along with the increasing awareness of health and good environment, the demand for environmentally friendly emulsifiers and easily degradable are increasing. One of emulsifier that meets these criteria is fatty acid esters of carbohydrates, because the ester is derived from material that is easily degraded and renewed [1]. Carbohydrate fatty acid esters can be synthesized from glucose and fatty acid chain usually 10C or more [2,3]. As an abundant commodity in Indonesia, coconut oil has a lot of potential. One is as a source of fatty acid. The highest fatty acid content of coconut oil is lauric acid (C12:0) that can be used for the synthesis of fatty acid esters of carbohydrates.

Synthesis of glucose ester can be done either chemically or enzymatically. Enzymatic reaction is generally preferred because it does not require extreme reaction conditions. Nevertheless, the enzymatic reactions cost very high because the enzymes used in the reaction cannot be retrieved and reused in the next cycle of reaction. One of the solutions for this problem is by immobilizing the enzyme on a non-soluble matrix. Enzyme modification by immobilization is widely used in industry. Immobilization of enzymes on an inert and insoluble matrix were known to have several advantages, among which tends to stabilize the structure of the enzymes thereby increasing the resistance of enzymes to the conditions of pH, temperature, and organic solvents [4]. Immobilization studies of lipase known also to enhance the catalytic activity for the esterification reaction and are able to maintain the catalytic activity until a few days after deposit [5,6,7].

Alginate, a natural polysaccharide, is one material that can be used as an immobilization matrix. Alginate has the ability to form a gel when reacted with divalent cations. Immobilization method using alginate can be done at room temperature. In this study, the *Candida rugosa* lipase was immobilized in Ca-alginate gel matrix. Studied include the influence of alginate concentration on the results of immobilization and influence of temperature, the ratio of glucose to fatty acids, incubation time, and the weight of molecular sieve enzymatic esterification reactions.

II. Materials And Methodes

2.1. Materials

The materials used were *Candida rugosa* lipase EC. 3.1.1.3. obtained from Sigma Aldrich (Singapore), Na-alginate obtained from Sigma Aldrich (Singapore), tris HCl, glucose monohydrate, and hexane obtained from Merck (Indonesia). Coconut oil was purchased from a super market in Jakarta. All chemicals have pa quality and used directly without further purification.

2.2. Methodes

2.2.1 Fatty acid composition of coconut oil.

Determination of fatty acid composition of coconut oil is done by standard methods GC analysis of fatty acid methyl ester form (FAME)

2.2.2. Hydrolysis of Coconut Oil.

A total of 20 g of coconut oil put in a three-neck round flask and then was added with 100 mL of 1.0 M KOH in 95% alcohol. The mixture was then heated by reflux system for 1 hr at 62 ± 2 °C and stirred by a magnetic stirrer. Once heated, the mixture was added by 50 mL of distilled water and 35 mL of HCl 3.0 N. The organic phase was extracted with 50 mL of n-hexane twice to remove fatty acids from water phase. Further into the organic phase was added 1.0 g Na₂SO₄ anhydrous and decantation to separate Na₂SO₄. Furthermore, the solvent n-hexane was evaporated using rotator evaporator until the resulting filtrate concentrated. The filtrate obtained was hydrolyzed fatty acids to be used in the subsequent experiments.

2.2.3. Immobilization of Lipase on Ca-alginate matrix.

The immobilized method used was a direct entrapment [8]. A total of 2.0 mL of lipase solution was mixed with 8 mL of Na-alginate to produce a ratio of enzyme/alginate (w/w) of 0.125. The mixture was stirred with magnetic stirrer to mix evenly. The solution was added dropwise using a syringe into 10.0 mL of 50.0 mM CaCl₂. Ca-alginate beads were formed for 20 minutes and then separated from the solution by vacuum filtration. The beads were washed on the filter twice with 50.0 mM Tris buffer solution HCl pH 7.2. Collected filtrate was analyzed to determine loading value of immobilized enzyme. This value was used to determine the number of mg of protein in Ca-alginate bead. Loading value was calculated by equation (1).

$$\text{Loading value (\%)} = \frac{C_i V_i - C_f V_f}{C_i V_i} \times 100 \quad (1)$$

C_i is the initial protein concentration and C_f is total protein concentration in the filtrate that was determined by Lowry method [9], while V_i is the initial volume of the protein and V_f is the total volume of filtrate.

Variations in Na-alginate concentrations used were 1.0 %, 1.5 %, and 2.0% (w/v). The optimum conditions were determined by the largest efficiency of immobilization. Immobilization efficiency values described how much immobilized enzyme in the matrix still has the catalytic activity and a benchmark of successful immobilization process. Immobilization efficiency values were calculated using equation (2).

$$\text{Immobilization efficiency (\%)} = \frac{a_{\text{imm}}}{a_{\text{free}}} \times 100 \quad (2)$$

a_{free} is the specific activity of free lipase, and a_{imm} is the specific activity of the immobilized lipase. The specific activity is defined as the immobile lipase activity per mg protein. The activity of free lipase and immobile lipase is determined by titrimetric method. The number of mg of protein in immobile lipase was determined from the loading value.

2.2.4. Optimization of Fatty Acid–Glucose Esterification.

Esterification reaction was carried out in 100-mL container. A total of 0.1 mmol of glucose was reacted with fatty acids of coconut oil hydrolyzate (1-9 mmol), with n-hexane as a non-polar solvent as much as 1:1 v/v substrate. Then the solution was added by 1.0 g lipase beads - Ca-alginate and molecular sieve (0 - 0.7 g) which was activated by heating temperature of 400 °C for 3 hours. The mixture was then shaken in a horizontal incubator shaker at 200 rpm at the desired temperature and time [10]. The reactions were terminated by heating at 80 °C.

Reaction carried triplo by variations in temperature, the ratio between the molar ratio of glucose and fatty acids, incubation time, and the weight of molecular sieve used. The variations in incubation time taken were 4, 8, 16, and 32 hours. The variations of the reaction temperature used were 30, 35, 40, and 45 °C. Variations in molar ratio of glucose and fatty acids used were 1:10, 1:30, 1:60, and 1:90. Variations of molecular sieve used were 0.0; 0.1, 0.4, and 0.7 g.

2.2.5. Analysis of Esterification Products.

Esterification reaction products were analyzed by titration method for determining the percent conversion of fatty acids and be repeated three times. Titration performed using NaOH solution. Percent conversion of fatty acids was determined by equation (3), [10].

$$\% \text{ Conversion} = \frac{(V_{\text{blank}} - V_{\text{sample}}) \times [\text{NaOH}]}{\text{mol fatty acid}} \times 100 \quad (3)$$

2.2.6. Separation and Identification of Esterification Products.

Separation of esterification products were done by centrifugation. This process was carried out with a speed of 3400 rpm for 15 minutes. Identification of products made using FT-IR instrumentation and emulsifier

test. Emulsifier test made by mixing approximately 1.0 mL of water with 10 drops of oil, then the addition of glucose ester synthesis results while continuing to be shaken and see the changes. When the emulsion was formed, it observes on the stability of the emulsion for 24 hours. For the determination of the type of emulsion formed was done by dripping a drop of emulsion on glass preparations. After that, the preparation was added by eosin. Testing was done by observation using a microscope to determine whether the emulsion that forms an emulsion of oil in water (o/w) or water-in-oil (w/o).

III. Result And Discussion

3.1. Coconut Oil Fatty Acids Composition.

The analysis results of fatty acids composition in coconut oil gave the maximum composition of Lauric acid (54.10 %). The average Mr of fatty acids is 207.89 that were used for mole calculation of fatty acid needed in experiment. Composition and its contribution to average Mr fatty acid as can be seen at Table 1.

Table 1. The fatty acid composition of coconut oil used and its contribution to average Mr.

Fatty Acid	Mr	Percentage(%)	Contribution to Mr
Caprylic(Oc, C8: 0)	144.0	7.20	10.37
Capric(D, C10: 0)	172.0	8.02	13.79
Lauric(L, C12: 0)	200.0	54.10	108.20
Miristic(M, C14: 0)	228.0	17.40	39.67
Palmitic(P, 10:0)	256.0	6.64	17.00
Stearic(S, C18: 0)	284.0	1.86	5.28
Oleic(O, C18: 1)	282.0	3.99	11.25
Linoleic(L, C18: 2)	280.0	0.81	2.27
Linolenic(Ln, C18: 3)	278.0	0.02	0.06
Average Mr			207.89

3.2. Triglyceride hydrolysis of coconut oil.

The hydrolysis of triglycerides of coconut oil performed under alkaline condition. Hydrolysis carried out using 95% KOH in alcohol gives better results and more soluble fatty acid salt in water than the results with NaOH [11]. The addition of water into the reaction mixture serves to separate saponification to unsaponification products. The product of reaction mixture, which was a potassium salt-fatty acid, was then converted into its acid form by the addition of excess hydrochloric acid and separated from the mixture by extracting with n-hexane. The results of the fatty acid are then used as substrates in subsequent experiments. Percent yield of hydrolysis was 92.80%.

3.3. Optimization of Candidarugosa Lipase Immobilized in Ca-alginate matrix.

Immobilization method of lipase in Ca-alginate bead matrix is a trapping method, namely entrapment of enzyme molecules in the cavities of alginate matrix. Ca-alginate beads are formed when sodium alginate solution is dripped into a solution of CaCl₂. This is due to the crosslinking between the divalent cations Ca²⁺ with carboxylate anions (-COO⁻) of the monomer guluronate (G) in the alginate molecules, forming a three-dimensional network in the form of a gel [12]. Immobilization of lipase in a matrix of Ca-alginate occurs when a solution of alginate is mixed with a solution of the enzyme lipase to form gel beads and because crosslinking between alginate with cations Ca²⁺ led to the formation of a gel. The two factors that affect the process of immobilization are the solution concentration of alginate used and the concentration of the solution CaCl₂ as a source of divalent cations [8]. Based on some research on the immobilization by Ca-alginate matrix, the concentration of CaCl₂ did not have a significant influence on the amount of enzyme trapped (loading value) as well as the efficiency of immobilization compared with the concentration of alginate. On the basis of this, in this study varied only the alginate concentrations are 1, 1.5 and 2%. The loading value and the immobilization efficiency by alginate concentrations can be seen in Fig. 1.

Based on the results obtained, the higher the concentration of alginate used, the higher the loading value, but the value of the immobilization efficiency decreased. This is because the anion alginate crosslinked with Ca²⁺ ions, the increase in the concentration of alginate cross allegedly makes connective tissue more and more. The amount of connective tissue makes the rate of diffusion to cross into or out through the smaller matrix [8,13,14]. The *Candida rugosa* lipase (56 kDa) can not diffuse out the matrix, so that the value loading is high. However, the rate of substrate diffusion into the matrix are also small, it makes difficult to reach the enzyme that makes in a small value of immobilization efficiency. Based on these results, it was found that

alginate concentration for the immobilization was 1.0 % (w/v) generate loading value and immobilization efficiency of 40.50% and 61.66%.

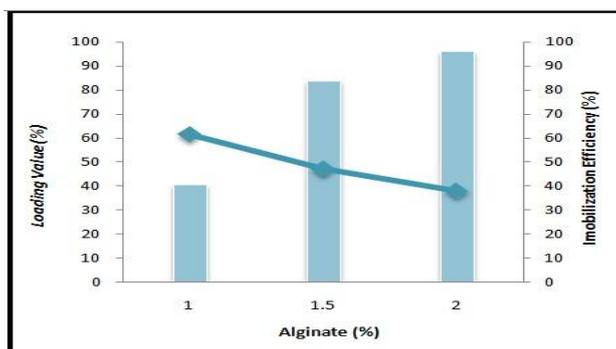


Figure 1. The effect of alginate concentration to the loading value (%) and the immobilization efficiency (%). The loading value (bar) and the immobilization efficiency (◆).

3.4. Optimization of Lipase Immobilized Ca-alginate in Esterification Reaction.

The purpose of immobilized lipase in Ca-alginate on the esterification reaction is the enzyme can be used repeatedly. This is supported by a previous study using Ca-alginate immobile lipase as biocatalyst esterification reaction [15].

To find out the esterification reaction, it analyzed by titrimetric indirectly by measuring the reduction of fatty acids in the reaction mixture [10].

In the enzymatic esterification reaction, there are some factors that influence the course of the reaction such as: solvents are used, the ratio of fatty acid substrate to glucose, temperature and pH buffer used. In this study, n-hexane used as solvent having a log P value of 3.5. Solvents with log P values ranging from 2 to 4 are selected on the esterification reaction. When used solvents with high log P value, may result in differences between the solvent polarity to glucose so the contact between the glucose to fatty acid is getting smaller. In the study of esterification by lipase is also known that the use of n-hexane as a solvent gave the best results [15,16,17]. The use of n-hexane solvent restricted 1:1 v/v substrate because if the ratio is too large can cause dehydration so lipase activity decreased. Reaction was performed at pH 7.2 in Tris-HCl buffer pH, it is in line to the results of previous studies that optimally between pH 6.5 - 7.5 [8].

Incubation temperature variations performed to determine the optimal temperature of the esterification reaction. The largest percentage conversion of the fatty acid was obtained at a temperature of 35 °C, Fig. 2a, according to the previous study shown that the lipase optimal temperature is between 30-35 °C [18]. Previous studies using the free enzyme get the optimum temperature at 30 °C. This is because the use of lipase immobilized on Ca-alginate gel matrix required a greater kinetic energy. Substrate ratio of glucose to fatty acids used was at least twice the number of carboxylic groups on the number of hydroxyl groups of the carbohydrate [19,20]. Used excess reactant ratios as expected the reaction equilibrium will shift towards the formation of the product. In addition, the magnitude of the ratio of fatty acids can also be non-polar system so as to minimize the water content in the system.

In this research, percent conversion increase with increasing ratio up to 1:60, but above that ratio, the percent conversion decreased; Figure 1b. High substrate concentration will increase the rate of reaction until it reaches the optimum limit. However, too high concentration of fatty acids can lead to free carboxylic acid groups or ionized high. This causes the water layer (essentially water) around the enzyme is acidic, so the lipase protein tertiary structure is unstable and tends to change on under normal conditions [15].

The optimal incubation time was 16 hours, Figure 2c. Decrease in percent conversion after 16 hours due to the amount of water formed causing mass transfer resistance immobile substrate of the enzyme [15]. Another cause is hydrolysis of ester product, so that the percent conversion was reduced.

Esterification reaction is an equilibrium reaction and one of its products is water. To that end, there should be decreased the water from the reaction mixture, one way is to use molecular sieve. In this study, the addition of molecular sieve turns causes a decrease in the value of percent conversion, Figure 2d. This was related to the physical form immobile lipase used. Ca-alginate gel matrix used for immobilization of lipase also has water content as a framework constituent gel. The greater of molecular sieve used would interfere with lipase immobile Ca-alginate. This is due to the power of molecular sieve dehydration is very large, resulting in water that make the water of the alginate gel is absorbed out of the alginate molecules. Molecular alginate matrix dehydrated causes to be damaged and result in decreased immobile lipase activity.

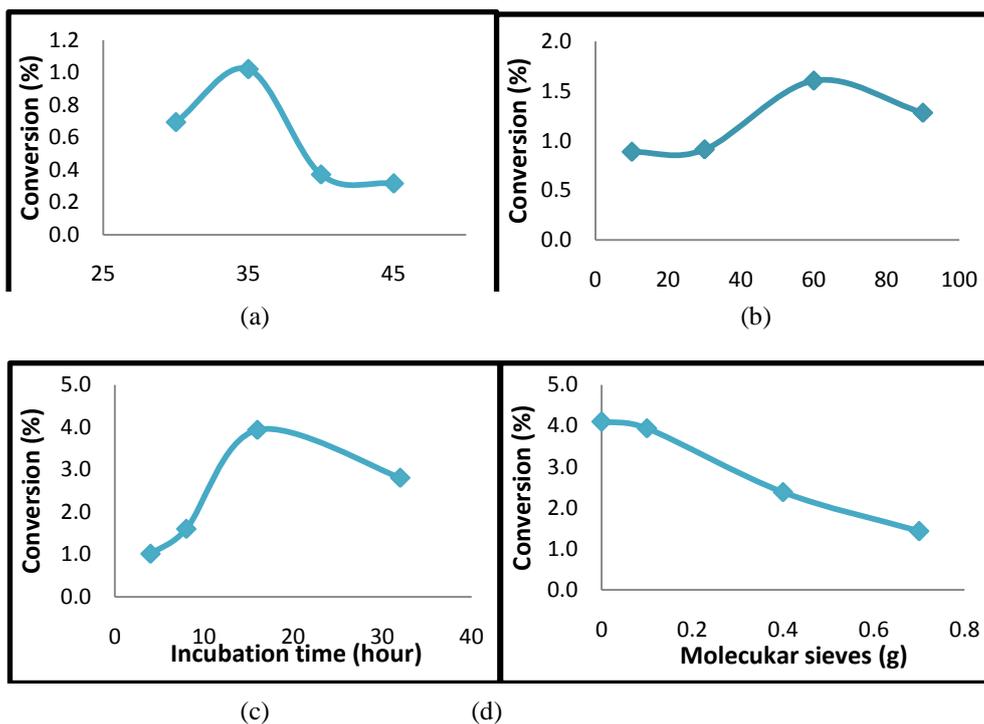


Figure 2. The effect of temperature (a), the ratio of the substrate G:FA (b), incubation time (c) and molecular sieve added (d) to the percent conversion of glucose-fatty acid esters.

3.5. Identification of Glucose Esters Products

Identification esterification products by FT-IR aim to look at the qualitative functional groups present in the compound. FT-IR spectra showed the appearance of absorption bands for ester groups in the region $1750 - 1735\text{cm}^{-1}$. The other is the absorption peak in the region $3500 - 3200\text{cm}^{-1}$ which is the absorption band of alcohol-OH group. It is meant that still indicates the presence of non-esterified hydroxyl groups, which suggests that glucose esters synthesis has a low degree of substitution. Fatty acid esters of carbohydrates are difficult to be synthesized enzymatically to produce products with a high degree of substitution [1]. Steric hindrance of carbohydrate used (glucose) is high enough; it can be seen from the number of primary-OH group that is only one piece, so that the esterification reaction to produce products with a high degree of substitution becomes difficult.

The product has a low degree of substitution and can be served as an emulsifier. Ester group is non-polar and unsubstituted hydroxyl group is the group of polar and more soluble in water. To prove this, a simple test of the product emulsion is formed, Figure 3a, b, and the observation of the emulsion system formed, Figure 3c. Based on observations with the microscope, it was known that the emulsion system formed was an emulsion of oil in water (o/w).

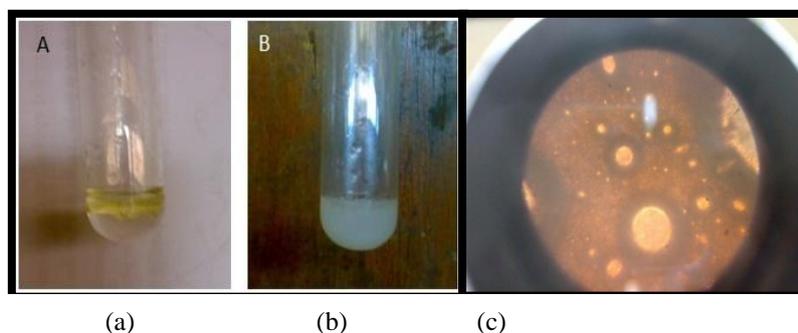


Figure 3. Simple emulsion test results prior to the addition of the reaction product (a) after addition of the reaction product (b) and the observation of emulsions formed with a microscope is known that the emulsion formed is an emulsion of oil in water (o/w).

IV. Conclusion

Lipase was successfully immobilized in Ca-alginate gel matrix. The immobilization of *Candida rugosa* lipase on Ca-alginate was found to be optimized when using 1% alginate solution, resulting 61,66% immobilization yield. The optimum conditions for esterification reaction were at 35°C, glucose fatty acid ratio 1:60 mmol, 16 hours incubation time, and without using molecular sieve.

Synthesis of glucose esters of fatty acids can be made using the results of hydrolysis of coconut oil catalyzed by immobilized *Candida rugosa* lipase on Ca-alginate. Identify products with FT-IR showed absorption peaks C=O ester group at wave numbers 1737.86 cm⁻¹, but with the great OH group absorption peaked at wavenumber 3344.57 cm⁻¹ indicates that the degree of esterification is still low. Based on the test emulsion, it is known that the reaction products glucose esters are compounds that have properties amphiphilic as an emulsifier and established as a system of oil-in-water emulsion (o/w).

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