# Removal of Yellow 2G dye from aqueous solutions using activated carbon prepared from mosambi and cotton an agricultural waste

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**Abstract :** Adsorption of Yellow 2G from aqueous solution on the surface of Activated carbon of mosambi peel (ACMP) and stem of cotton (ACCS) was accomplished under the optimize conditions of pH, adsorbent dose, initial concentration of dye and contact time. Spectrometric technique was used for the measurements of concentration of dye before and after adsorption. Colour was effectively been removed at all selected pH, and the increase in activated carbon dose showed an increase in the removal's percentage. The result shows that the removal efficiency increases with adsorbents dose increases and at neutral pH. The equilibrium data fit well with both Langmuir and Freundlich models of adsorption. The value of separation factor  $R_L$  for ACMP and ACCS was found to be 0.135 and 0.080 respectively suggesting that the isotherm to be favorable at the concentration studied. The results of findings are discussed to reflect the removal efficiency of adsorbent. **Keywords:** Yellow 2 G, Mosambi Peels, and Stem of Cotton, Adsorption, Langmuir and Freundlich isotherm.

# I. INTRODUCTION

Dyes production industries and many others industries which used dyes and pigments generated wastewater, characteristically high in colour and organic content. Most of the industries such as textile, paper, carpet, and printing use dyes and pigments to color their products. Due to their good solubility, synthetic dyes are common water pollutants and they may frequently be found in trace quantities in industrial wastewater. However, the discharge of dye-bearing wastewater into natural streams and rivers possess a severe problem, as dyes impart toxicity to aquatic life and are damaging the aesthetic nature of the environment. In order to preserve the physical and ecological properties of the receiving water bodies and the environment it is necessary to remove dyes from waste water. Among various physical and chemical methods used for removal of dyes, adsorption has shown better decontamination efficiencies. Activated carbons are widely known for their high absorption capacity, however, high operating cost hamper their use in large scale applications [1]. This has prompted many researchers to search for cheaper substitutes such as babul Seed [2], barley husk [3], sunflower stalks [4] and the peel of cucumis sativa fruit [5], orange peel and lemon peel [6] were used as adsorbent. Consequently, a low cost and easily available material such as mosambi peels can be studied for the removal of different dyes from aqueous solutions at different operating conditions. Mosambi was easily available fruit in local area in bulk quantity and its peels were used to prepare adsorbent for the dye removal. Previously the work on removal of textile Erichrome black T dye from aqueous solution from aqueous solution by adsorption technique using natural waste was investigated in this laboratory. [7-9] In the present investigation, we used mosambi peels and stems of cotton as a raw material to produce activated carbon to remove the Yellow 2G dye from water.

## 2.1 Adsorbate

# II. MATERIALS AND METHOD

Stock solution (1000 mg/l) of Yellow 2G Dye was prepared by dissolving 1g of dye in 1000 mL of double distilled water. The stock solutions were diluted with double distilled water to obtain required standard solution.<sup>92</sup> Batch adsorption studies were performed at room temperature  $(39\pm1^{\circ}C)$ . TABLE 1 enlists the properties of Yellow 2G Dye used.

## 2.2 Adsorbents

The mosambi peels and stems of cotton were collected from local area of Jalgaon district in clean plastic bags. These waste materials are washed with distilled water, dried in sunlight, then 60°C for 24 hours in hot air oven. The dried material was subjected for acid treatment (ratio 1:1) and kept at room temperature overnight and stored in a tight lid container for further studies. It is then screened through a mesh sieve with a particle size range of 180-300  $\mu$ m. Carbon was prepared by treating air-dried prepared fresh natural adsorbents with concentrated sulphuric acid in a weight ratio of 1:1 for 24 hours. The resulting black product was kept in an air-oven maintained at 105°C for 12 hours followed by washing with NaHCO<sub>3</sub> and water until free from excess acid and dried at 105±5 °C to get mosambi peel activated carbon and activated carbon of stem of cotton. Product

obtained was ground well to fine powder and the physical properties are analyzed by usual standard methodologies.

# 2.2 Batch adsorption studies

Adsorption experiments were performed at room temperature  $(39\pm1^{\circ}C)$ , 0.004 g/ml of adsorbent was mixed with known initial dye concentration (50, 100, 150, 200 and 250 mg/l respectively) 100 mg/l dye solution was used for adsorbent dose variation study. For pH variation, 100 mg/l dye solution with 0.004 g/l adsorbent dose was used. The adsorbent and adsorbate were separated by filtration and filtrate was analysed for residual Yellow 2G concentration spectrophotometrically using UV Visible spectrophotometer (Systronic, Model No. 166) at  $\lambda_{max}$ = 340 nm.

# III. **RESULTS AND DISCUSSION**

3.1 Characteristics of the adsorbent The physico- chemical properties of the prepared activated carbon were determined by standard procedures. Surface area was determined by BET method. The physico- chemical properties are listed in TABLE 2.

# **3.2 Effect of Dye Concentration:**

To study the effect of different initial concentrations of Yellow 2G on adsorption behaviour, five concentrations (50, 100, 150, 200 and 250 mg/L) were used and the amounts adsorbed were calculated and given in TABLES 3-4. The observed increase in the adsorption of Yellow 2G with increase in concentration may be due to sufficient adsorption sites at adsorbent. The amount of dye adsorbed (mg/g) increased with increase in time and the equilibrium for dye removal attainment was achieved after 120 min. The initial dye concentration provides the necessary driving force to overcome the resistances to the mass transfer of Yellow 2G between the aqueous and solid phases. The maximum adsorption is obtained by ACMP and ACCS which is 88.78 % and 92.14 % respectively. [10]

## 3.3 Effect of adsorbent dose variation:

The effect of adsorbent dose on removal of yellow 2G was studied by varying the dose of adsorbent (0.002, 0.004, 0.006, 0.008 and 0.01 g/L) in the test solution while keeping the initial dye concentration 100 mg/L (Temperature  $39\pm1^{\circ}$ C) at pH=7. Experiments were carried out at different contact times for 120 mins. Tables 3.22 - 3.27 reveal that percent of adsorption increased with increasing adsorbents doses. The increase in the percent removal of dye with the increase in adsorbent dosage is due to the availability of larger surface area with more active functional groups. The maximum adsorption yellow 2G is by ACMP and ACCS which is 92.68 % and 94.12 % respectively. [11]

## 3.4 Effect of pH variation

Adsorption is also affected by change in pH of the solution as shown in Fig 1. The hydrogen ion concentration (pH) primarily affects the degree of ionization of the dye and the surface properties of the adsorbents. Experiments were carried out at 100 mg/L initial dye concentration with 0.004 g/L adsorbent mass at room temperature ( $39 \pm 1^{\circ}$ C) for 3 hour equilibrium time. It is clear from the Fig 1 that for each initial concentration value of yellow 2G, the percent removal increases as pH rises and after pH 7.0, the percent removal decreases with further increase in pH value. This clearly shows that the optimum pH for the present adsorbate-adsorbent system is 7.0.<sup>[12]</sup>

## 3.5 Adsorption Isotherm:

The experimental data are analyzed according to the linear form of the Langmuir and Freundlich isotherms.

The Langmuir isotherm is represented by the following equation

 $(Ce/qe) = (1/Qob) + (Ce/Qo) \dots (1)$ 

Here Ce is the equilibrium concentration (mg/L), qe is the amount adsorbed at equilibrium (mg/g). Qo and b is Langmuir constants related to the adsorption efficiency and energy of adsorption, respectively. [13]

The linear plots of Ce/qe versus Ce suggest the applicability of the Langmuir isotherms are given in Figures 2 and 4 for ACMP and ACCS respectively. The values of Qo and b were determined from slope and intercepts of the plots and are presented in TABLE 7.

The essential characteristics of the Langmuir isotherm can be expressed in terms of a dimensionless constant separation factor RL that is given in Eq.2.

 $R_L = 1 / (1 + bCo)$  ------(2)

The value of RL indicates the type of the isotherm to be either favorable (0 < RL < 1), unfavorable (RL > 1), linear (RL = 1) or irreversible (RL = 0). The value of RL was found to be the values of RL were found between 0 and 1 for ACMP and ACCS suggesting the isotherm to be favorable at the concentrations studied. [14]

The Freundlich equation is also employed for the adsorption of Poly Acid Brill Red 3 BN on the ACMP and ACCS adsorbent. The Freundlich isotherm (Freundlich, 1906) is represented as  $\log qe = \log kf + (1/n) \log Ce$  ......(3)

Here qe is the amount of yellow 2G dye adsorbed (mg/ g), Ce is the equilibrium concentration of dye in the solution (mg/L) and Kf and n are constants incorporating all factors affecting the adsorption capacity and intensity of adsorption, respectively. Linear plot of log qe versus log Ce shows that the adsorption of yellow 2G follows also the Freundlich isotherm (Figure 3 and 5 for ACMP and ACCS respectively). The values of Kf and n given in the Table 7. As seen from Table 7, the increase in negative charges on the adsorbent surface that makes electrostatic forces like Vander Waals between the adsorbent surface and dye ion. The molecular weight, size and radii either limit or increase the possibility of the adsorption of the dye onto adsorbent. However, the values clearly show the dominance in adsorption capacity. The intensity of adsorption is an indicative of the bond energies between dye and adsorbent and the possibility of slight chemisorptions rather than physisorption. However, the multilayer adsorption of yellow 2G through the percolation process may be possible. The 'n' value was 1.9305 and 2.1739 was in between 1 and 10 indicating the adsorption is much more favourable for a selected adsorbents. [15]



Figure 2: Langmuir isotherm for the removal of Yellow 2G by ACMP

Ce







Figure 5: Freundlich isotherm for the removal of Yellow 2G by ACCS

TABLE 1 Characteria	stic of Yellow 2G Dye
Molecular Formula	$C_{16}H_{10}Cl_2N_4Na_2O_7S_2$

Molecular Formula	$C_{16}H_{10}Cl_2N_4Na_2O_7$
CAS number	6359-98-4
CI Number	18965
Water Solubility	100 g/l

Sr No. Properties		operties Mosambi Peel Activated Carbon			
1	pH	7.7	7.3		
2	Moisture Content (%)	6	7		
3	Ash Content (%)	23	24		
4	Apperent Density (g cc <sup>-1</sup> )	0.5494	0.431		
5	Solubility in water (%)	0.34	0.54		
6	Solubility in HCl (%)	0.89	1.78		
7	Surface area (m <sup>2</sup> g <sup>1</sup> )	189	198		

**TABLE 2:** Characteristic of activated carbons of mosambi peels and stem of cotton.

**TABLE 3:** Effect of different initial dye concentration on dye removal using ACMP (Adsorbent dosage=400mg/50mL, initial pH=7.0, time = 120 min size = 180 -300 micron)

Turiti-1.1	Percentage of dye removal with time (min						
Initial dive concentration (mg/L)	15	30	45	60	90	120	
50	26.42	49.06	56.60	73.58	86.79	88.68	
100	28.57	45.92	62.24	80.61	87.76	88.78	
150	32.14	48.57	65.00	78.57	87.86	88.57	
200	35.33	49.46	61.41	78.80	88.04	88.59	
250	38.01	53.85	60.18	76.92	88.24	88.69	

**TABLE 4:** Effect of different initial dye concentration on dye removal using ACCS (Adsorbent dosage=400mg/50mL, initial pH=7.0, time = 120 min. Size = 180 -300 micron)

Toritic I does no support to the second second	Fercentage of dye removal with time (n							
Initial dye concentration (mg/L)	15	30	45	60	90	120		
50	22.64	37.74	60.38	73.58	88.68	90.57		
100	24.49	39.80	57.14	72.45	88.78	89.80		
150	32.86	52.14	70.00	81.43	90.71	92.14		

**TABLE 5:** Effect of different concentration of ACMP on dye removal (Dye concentration= 100 mg/l, initial pH=7.0, time = 120 min., size = 180 -300 micron)

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Ad sorbent dose (g/100mL)		Percentage of dye removal with time (min)							
Ads	orment a ose (g/100mL)	15	30	45	60	90	120		
	0.2	21.14	34.15	45.53	62.60	70.73	73.17		
	0.4	28.57	45.92	62.24	80.61	84.69	84.69		
	0.6	35.44	54.43	64.56	79.75	86.08	87.34		
	0.8	41.79	59.70	76.12	82.09	88.06	88.06		
	1	29.27	53.66	68.29	80.49	90.24	92.68		

**TABLE 6:** Effect of different concentration of ACCS on dye removal (Dye Concentration= 100 mg/l, initial<br/>pH=7.0, time = 120 min., size = 180 -300 micron)

Aland and I am (= 0.00 an I )	Percentage of dye removal with time (min)							
Aasomentaose (g/100mL)	15	30	45	60	90	120		
0.2	20	19.13	25.22	46.96	66.09	67.83		
0.4	24.49	39.80	57.14	72.45	88.78	89.80		
0.6	24.36	47.44	61.54	75.64	87.18	87.18		
0.8	14.52	25.81	50.00	77.42	90.32	90.32		
1	27.45	43.14	58.82	78.43	92.16	94.12		

**TABLE 7:** Langmuir and Freundlich isotherm of activated carbon prepared from various
 materials for Yellow

 2G
 2G

Adsorbents		Langn	uir iso therm		Fre	undlich i	sotherm
	Qo	b	Correlation coefficient (r)	RL	Intercept (kt)	Slop e (1/n)	Correlation coefficient (r)
ACMP	24.390	0.0448	0.825	0.135	0.348	0.518	0.915
ACCS	18.867	0.0803	0.939	0.080	0.433	0.46	0.864

V.

# CONCLUSION

The present study revealed that activated carbon prepared from natural waste like peels of mosambi and stem of cotton could be employed as a potential adsorbent for the removal of Yellow 2G dye. The adsorption of Yellow 2G was found to be dependent on the pH, contact time, initial concentration and adsorbents dosage. The experimental data of Yellow 2G was analyzed according to the linear form of the Langmuir and Freundlich isotherms. The adsorption obeyed both Langmuir and Freundlich isotherms for selected adsorbents such as peels of Mosambi and stems of Cotton. The characteristic parameters for each isotherm and related correlation coefficients were determined from graphs of their linear equations. Both Langmuir and Freundlich isotherms were demonstrated to provide a meaningful correlation for the adsorption of dye on to activated carbon prepared from natural waste. The advantage is twofold; it not only acts as an effective and economic tool as compared to other existing commercial carbons for solving the problem of dye pollutions but also helps in an effective and useful disposal of natural waste from local area.

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