

Gas Turbines Waste Heat/Power Recovery in Tropical Climate Zones: Analysis to Inform Decision Making.

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Abstract: Gas turbines (GTs) are commonly used in the power generation field. In some applications, it is the preferred option due to its compactness and low weight. Site conditions especially ambient temperature has a strong influence on the gas turbine performance. The gas turbines power plant that is currently under operation in northern kingdom of Saudi Arabia consists of 7 gas turbine of 25MW each. In this area, during summer season, the ambient temperature may reach 50 °C when peak demand occurred, resulting in lower power output and consequently, the problem of electricity black-out occurs unless power demand is decreased. The present paper is mainly prepared to support GTs plant decision makers (technically and economically). A mathematical model was prepared firstly to study the effect of site conditions on the performance of the above mentioned GTs plant. Secondly, the investment cost to add an absorption chiller is to be justified. The results showed that, about 20% of the power output is lost due to increasing the ambient air temperature, from 15 oC (design conditions) up to 50 °C (actual site conditions). Moreover for hot climate countries, adding an absorption chiller for existing GT plants is strongly recommended which is financially justified (payback period=1.14 year or less). Finally, for future GT power plants, gas turbines with inlet air cooling are advised for hot climate zones.

Keywords: Gas turbines power plants, power loss, hot climates, and analysis.

I. Introduction

The operation of a GT is based on the Brayton cycle (Figure 1), where fuel is mixed with compressed air (fuel oil or natural gas) and burned under constant pressure conditions. The resultant hot gas expands through a gas turbine to produce a mechanical work. More than 50 percent of the turbine output power is consumed by the compressor. The simple cycle is the most basic operating cycle of gas turbines with plant efficiencies ranging from about 30% to 40% (8968-11606 kJ/kWh)[1-8]. In some cases of designs, to assure easy starting of GT, two bleeds are fitted at the 6th and 11th stage of the compressor. They remain open during the start up to 90% of the design speed [1-8]. Production capacities of GTs are rated by the International Standards Organization (ISO): Air inlet conditions: air temperature 15C, 60% RH, absolute Pressure 101.325 KPa. Such conditions are not applicable in hot climate zones, especially in summer. The difference between the ISO standard conditions of 15 C and the hot summer peak periods of approximately 40C, may result in a 20% drop in GT output[1-16]. Some researches [17-53] were focused on cooling the inlet air for power augmentation. Environmental issues like NO_x reduction using bypass air and catalyst systems were focused by other researches [54-77]. Using new catalytic combustors, the future target of NO_x emission is 2 ppm. Also for future plants, CO₂ capture and storage system is included[59,69]. Finally, integration between solar energy and GTs were studied for future applications [53-69].

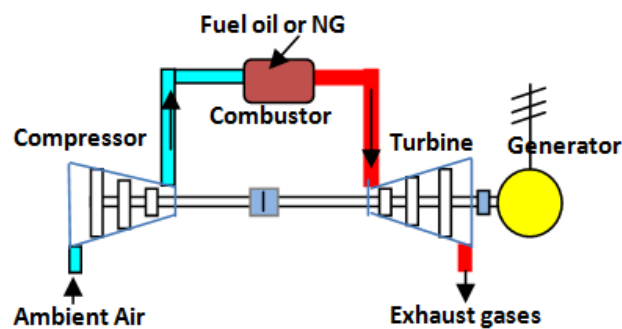


Figure (1): Gas Turbine Simple Cycle [3]

Generally, to increase the gas turbine specific power output, the researchers and designers has been focused on[9]:

- Increasing firing temperature
- Increasing pressure ratio
- Improving component design, cooling and combustion technologies, and advanced materials
- Technology transfer from aircraft gas turbines to stationary gas turbines for power generation and conversion of aircraft gas turbines to power generation applications
- System integration (e.g. combined cycles, inter-cooling, recuperation, reheat, chemical recuperation).

This paper presents a theoretical study to recover the power loss due to high ambient temperature by using a flue gas heat recovery system. The study is mainly prepared to support decision makers either technically or economically. A mathematical model was prepared firstly to study the effect of ambient temperature on the performance of the above mentioned GTs plant. Secondly, the investment cost to add an absorption chiller is to be justified technically and economically.

II. Mathematical Model[1-16]

In this study, the selected actual gas turbine (TG 20) from FIAT-AVIO[2], with a nominal rating of 25 MW, is an open cycle and a single shaft gas turbine shown in fig.(2).

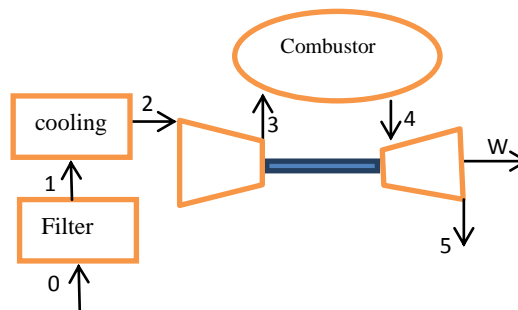


Fig.(2):Schematic of simple GT with inlet cooling

According to the flow direction through GT components, with the aid of fig.(2), the mathematical model is arranged as given below:

2.1 Inlet air cooling

Knowing the pressure drop through the inlet duct ΔP_{inlet} , the compressor inlet pressure can be calculated as follow:

$$P_2 = P_{atm} - \Delta P_{intake} \quad \text{-----1}$$

Where P_{amb} is the local atmospheric pressure

a-Inlet air cooling using evaporative Cooling system

The water cooler is modeled as an adiabatic air washer that delivers air to the compressor at saturation (about 100% relative humidity). The air exit temperature (T_{db2}) is related to both the ambient air temperature (T_{db1}) and relative humidity and can be calculated as follow:

$$T_{db2} = T_{db1} - \varepsilon (T_{db1} - T_{wb1}) \quad \text{----2}$$

Where

ε is the effectiveness of evaporative cooling process,

T_{db1} is the ambient air dry bulb temperature,

T_{wb1} is the ambient air wet bulb temperature.

b- Using absorption chiller

The cooling load (\dot{Q}) removed from the air flowing at ambient conditions into the power plant can be estimated as follows:

$$\dot{Q}_a = \dot{m}_a C_{pa} (T_1 - T_a) \quad \text{-----3}$$

Where

- \dot{m}_a air mass flow rate, Kg/s

- C_{pa} is the specific heat of the dry air at constant pressure,

- T_a is the ambient air temperature, C

T_1 is the temperature at the compressor inlet which should not be lower than 5°C in order to avoid condensation and freezing conditions.

The power required to operate the chiller is estimated from the following relation:

$$W_{ac} = \frac{Q_{coil}}{COP} \text{ -----4}$$

Where :

COP is the coefficient of performance of the employed chiller. Then, the output net power of gas turbine will be reduced as follows:

$$W_{net} = W_t - W_c - W_{ac} \text{ -----5}$$

2.2 Compressor

For a certain pressure ratio r_p , the fluid pressure at compressor outlet can be calculated using the following equation:

$$P_2 = r_p \cdot P_1 \text{ -----6}$$

Where inlet pressure entering the compressor is:

$$P_1 = P_{atm} - \Delta P_{intake}$$

The compressor isentropic efficiency can be evaluated using the following empirical equation:

$$\eta_{compressible} = 1 - \frac{[0.09 + (r_p - 1)]}{300} \text{ -----7}$$

The isentropic outlet temperature leaving the Compressor is determined from the following equation:

$$T_{2s} = T_1 (r_p)^{\frac{k_a - 1}{k_a}} \text{ ----8}$$

The isentropic temperature rise is determined from the following equation:

$$T_{Sr} = T_{2s} - T_1 \text{ ----9}$$

The actual temperature rise in the compressor is calculated from the definition of isentropic efficiency:

$$T_{ar} = \frac{T_{Sr}}{\eta_s} \text{ -----10}$$

Then, the actual outlet temperature leaving the compressor is:

$$T_{2a} = T_1 + T_{ar} \text{ ----11}$$

The actual work consumed by the compressor is given by:

$$W_c = \dot{m}_a C_{pa} T_{ar} \text{ ---12}$$

2.3 Combustor

The outlet pressure from the combustor is determined using the following equation:

$$P_3 = P_2 - \Delta P_{combustor} \text{ ----13}$$

Fuel mass flow rate is determined from the following equation:

$$\dot{m}_f = \frac{Q_{in}/HHV}{\eta_{Combustion}} \text{ ----14}$$

fuel/air ratio (F/A) is determined from the following equation:

$$F/A = \frac{\dot{m}_f}{\dot{m}_a} \text{ ----15}$$

heat input to the combustor can be estimated from energy balance across the combustor:

$$\dot{Q}_c = \dot{m}_a C_{pg} (T_3 - T_{2a}) \text{ ----16}$$

2.4 Turbine

At invariable turbine inlet temperature T_3 and pressure P_3 , The turbine isentropic efficiency can be estimated using following empirical equation:

$$\eta_{turbine} = 1 - \frac{[(T_3/P_3) - 1]}{250} \text{ ----17}$$

Where Outlet pressure at the turbine's exit is:

$$P_4 = P_{atm} + DBP \text{ ---18}$$

The expansion ratio is determined from the following equation:

$$r_{p1} = \frac{P_4}{P_3} \text{ -----19}$$

The isentropic outlet temperature leaving the turbine is determined from the following equation:

$$T_{4s} = T_3 (r_{p1})^{\frac{k_g - 1}{k_g}} \text{ ----20}$$

The isentropic temperature drop is determined from the following equation:

$$\Delta T_{4s} = T_3 - T_{4s} \text{ ----21}$$

The actual temperature drop is obtained from the definition of turbine's isentropic efficiency:

$$\Delta T_{4a} = \Delta T_{4s} / \eta_{\text{turbine}} \text{ -----22}$$

The actual outlet temperature leaving the turbine is determined from the following equation:

$$T_{4a} = T_3 - \Delta T_{4a} \text{ ---23}$$

The total mass flow rate is given by:

$$\dot{m}_{\text{tot}} = \dot{m}_f + \dot{m}_a \text{ ----24}$$

The work produced from the turbine is determined by the following equation:

$$W_T = \dot{m}_{\text{tot}} C_{pg} T_{4a} \text{ ---25}$$

The power output from the gas turbine power plant is:

$$W_{\text{net}} = W_T - W_c \text{ ----26}$$

The thermal efficiency without cooling intake air before being introduced to the gas turbine unit is:

$$\eta_{\text{th}} = \frac{W_{\text{net}}}{Q_{\text{in}}} \text{ -----27}$$

2.5 Economic analysis (assuming the cooling system to work only 2 months /year)

The refrigerated cooling systems can lower the air inlet temperature by about 25-30C. The economic study for adding such system to the existing plant is estimated below with the aid of table(1):

-yearly saving of electricity

Based on an amount of power output increase of 20% for two months per year (July and august)=0.2 x7units x25000 KW/turbine x60days/year x24hr/day= 50x10⁶ Kwh/year

-yearly saving in \$ =50x10⁶ Kwh/year x 0.12 \$/KWh= 6 x 10⁶ \$/year

- Initial Cost of adding absorption chiller=195.74\$/KW increase in power x 0.2x7unitsx25000 KW each=685.09x10⁴ \$

-Assuming lifetime is 10years, and then the cash flow diagram can be represented below in Fig.(3):

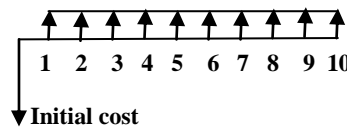


Fig.(3):Simplified Cash Flow diagram.

The financial key indicators are:

-Payback period=investment cost/ saving annually=685.09x10⁴ /6 x 10⁶ =1.14 years which is highly attractive.

- The other financial indicators can be calculated based on the CFD mentioned above (such as Net present value and internal rate of return).

Cooling system type	Percent increase in Power (%)	Cost,\$/KW increased
Evaporative cooling	3.32% x110 MW=3.69MW	135.67
Refrigeration inlet cooling	11.51%x110MW =12.77MW	2.5x10 ⁶ \$/12.77x10 ³ = 195.74

Cooling system type	Fuel saving per year,\$	Increase in sales revenue per year,\$	Total saving per year,\$
Evaporative cooling	515,264	396,755	912,019
Refrigeration inlet cooling	605,075	1,379,901	1,984,977

Table(1): cost and saving data for adding cooling system at inlet to compressor[Based on : GT operating at power=110MW, inlet temperature=32C, efficiency=32.92%, HR=10935KJ/KWhr[1].

III. Assumptions

- 1-The working fluid passing through the compressor is considered as an ideal mixture of air and water vapor, while that passing through the turbine is assumed to be an ideal mixture of combustion gases .
- 2-The ISO standard conditions are: 59 °F(15C), 60% relative humidity and 14.7 psia.
- 3-intake pressure drop (ΔP_{intake}) is taken to be 1 kPa, while the intake temperature is the same as the ambient temperature.
- 4-Specific heat ratio for air $K_a=1.4$ and specific heat for air $C_{pa} = 1.005$ KJ/Kg.K
- 5-Specific heat of flue gases, $C_{pg} = 1.15$ KJ/Kg.K, specific heat ratio of exhaust gas $K_g=1.332$
- 6-combustion efficiency ,
- $\eta_{Combustion} = 0.99$, pressure drop in the combustor $\Delta P_{combustor} = 48$ KPa
- 7-Diesel fuel higher heating value is assumed to be around 42 MJ/kg
- 8-Turbine design back pressure (DBP)=1 KPa

IV. Solution Technique

Gas turbine performance can be estimated using performance curves and site data at both full load and part load (i.e., elevation, ambient temperature, inlet and exhaust pressure drops, and the type of fuel). The set of equations (1-27) are used in calculating the GT performance using Engineering equations solver (EES) software.

V. Results And Discussion

The GT power plant performance is estimated based on actual values of site conditions and gas turbine engine characteristics. The power plant performance is characterized by net power output and heat rate.

5.1 Site Conditions [16-21]:

The max daily temperature for a complete year for Skaka city located in northern Saudi Arabia are given in table(2) [8]. Other parameters related to saturation condition can be obtained using Psychrometric chart.

	T_{amb}°C , daily maximum
Jan	22.7
Feb	27.6
March	33.8
April	41.8
May	48.6
June	52.2
July	55.1
August	55.8
Sept.	51.7
Octob.	42.5
Nov.	30.5
Dec.	23.7

Table(2)Maximum Of The Daily Earth Temperature (°C)(SKAKA City, Lat 29.97 , Lon 40.21)[5].

5.2 Effect of Inlet Air Cooling Systems

Cooling the air at compressor intake helps in increasing the density of air flowing into the GT plant and consequently increasing the generated power from the turbine. Fig.(4) illustrates the effect of compressor inlet temperature (T_2) on power output factor. Let the power output at ISO conditions ($T_{ambient}=15$ C) is 100% (factor =1). Then, from fig.(5)It is clear that the increase of ambient temperature from 15 C to 50 C leads to decrease in power output down to 77.5% .

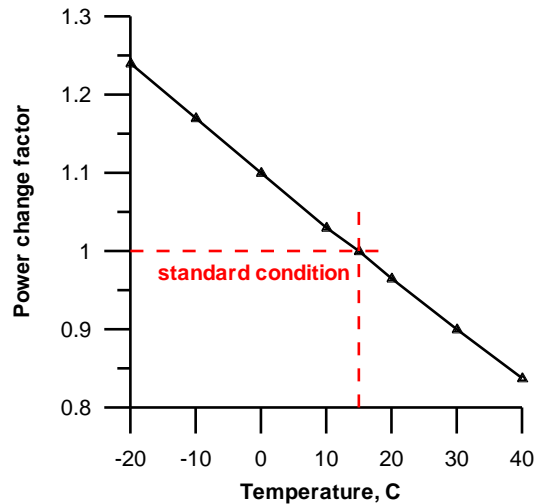


Fig.(4): Effect of compressor inlet temperature (T_2) on power output factor ($w_n/ W_n @ ISO condition$). The red arrowline points to the ISO condition(i.e $T_2=15 C$).

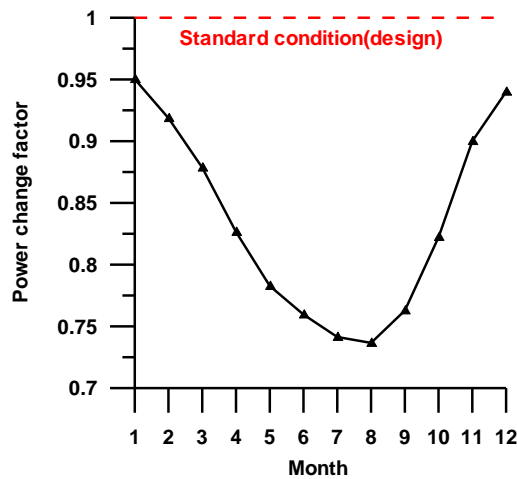


Fig.(5): variation of power change factor with site maximum daily temperature (Estimated monthly at max. daily temperature for SKAKA City[5].

As illustrated in fig.(5), During summer season in SKAKA area, the ambient temperature reaches it max in july and august, when peak demand occurred, resulting in deviation of the plant power from its design conditions (decreased to 78% of design conditions). Consequently, the problem of electricity black-out occurs. So, using the air cooling at compressor inlet is highly recommended

5.3 Verification of the obtained results

As discussed above, the increase in air temperature at inlet of GT compressor, causes a significant reduction in output power, especially in hot climate countries during summer. To verify the obtained results, a comparison with similar results obtained from GT manufacturers (table-3) is made. As shown in fig.(6), a good agreement is noticed between the results obtained from the present study and the GT manufacturers Data.

T_i, C	Power change factor
-20	1.24
-10	1.17
0	1.1
10	1.03
15	1
20	0.965
30	0.9
40	0.8375
50	0.775

Table.(3):influence of compressor inlet temperature on power output(base rating) (constant ambient pressure, turbine inlet temperature, and rotating speed)[76].

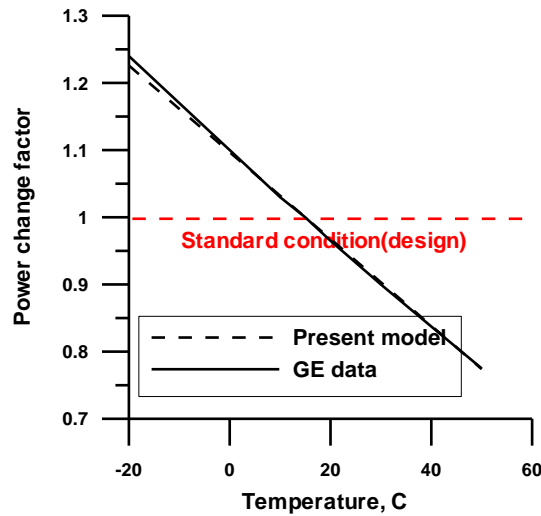


Fig.(6): comparison with similar results obtained from GT manufacturers.

From table(3), as the ambient temperature decreased from 50 C up to 15 C , the net output power increases from 78% of design value up to 100%. Consequently, say 20% increase in power (7units) means adding of 35 MW of power output to overcome the blackout problem during peak load.

5.4 Financial analysis results:

- As estimated in section II.5, the Initial investment Cost of adding absorption chiller=195.74\$/KW increase in power x 0.2x7unitsx25000 KW each=685.09x10⁴ \$
- yearly saving in \$ =50x10⁶ Kwh/year x 0.12 \$/KWh= 6 x 10⁶ \$/year
- Payback period=investment cost/ saving annually=685.09x10⁴ /6 x 10⁶ =1.14 years which is highly attractive.

VI. Conclusion

The present study is prepared, regarding power loss recovery for the existing units of GTs due to high ambient conditions. This is achieved by cooling the inlet air using a flue gases heat recovery system. It is concluded that:

- The ambient temperature has a strong influence on the gas turbine output power. As a Summary retrieving of power up to 20% is possible in hot climate zones.
- For tropical climate zones, adding absorption water chiller to the existing gas turbine for heat/power recovery is technically and economically justified. Also, for the new GT plant , it should be considered.

Nomenclature:

- GE General Electric
- GT Gas Turbine
- ISO International Standard Organizations
- C_{pa} Specific heat for air (kJ/kg. °K)
- C_{pg} Specific heat of the flue gas (kJ/kg. °K)
- COP Coefficient of performance of the mechanical chiller
- DBP Design back pressure (kPa)
- HHV Diesel fuel High Heating Value (MJ/kg)
- F/A Fuel to air mass ratio
- h Specific enthalpy(KJ/Kg)
- k Specific heat ratio
- \dot{m}_a Air mass flow rate (kg/s)
- \dot{m}_f Fuel mass flow rate (kg/s)
- \dot{m}_{tot} total mass flow rate (kg/s)
- P_{atm} Atmospheric pressure (kPa)
- TIT turbine inlet temperature (°C)
- η efficiency

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